

PREPARATION METHOD OF NZVI-PVDF HYBRID FILMS WITH CATION-EXCHANGE FUNCTION FOR REDUCTIVE TRANSFORMATION OF Cr(VI)

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Received 06 February 2017; accepted 02 June 2017

Abstract. Poly (vinylidene fluoride) (PVDF) microporous film was successfully synthesized and functionalized by poly acrylic acid (PAA) for immobilization of nanoscale zero-valent iron (NZVI). PAA was innovatively introduced onto PVDF film via *in situ* polymerization of acrylic acid (AA) and followed by ion exchange procedure. The as-prepared PAA/PVDF-NZVI hybrids (PPN) were characterized in terms of morphology (SEM) and surface functional groups (FTIR). FTIR spectra confirms the functionalization of PVDF film by coating of PAA within its micropores. And SEM images suggested that NZVI were well immobilized onto the surface of the support. Over the reaction course, the resultant PPN hybrids demonstrated high reactivity, excellent stability and reusability for Cr(VI) removal. Results showed that lower pH and initial concentration facilitated the removal of Cr(VI) by PPN. Compared with bare NZVI, PAA/PVDF film-immobilized NZVI resulted in a lower activation energy for Cr(VI) removal, indicating that Cr(VI) reduction process with PPN is a surface-controlled chemical reaction. Moreover, a two-parameter pseudo-first-order model was provided and well-described the reaction kinetics of Cr(VI) over PPN under various conditions.

Keywords: polyvinylidene fluoride, cation exchange function, hydrophilization, Cr(VI) removal, nanoscale zero-valent iron, revised kinetics, wastewater management.

Introduction

The widespread use of toxic heavy metals in industrial processes constitutes the primary source for water pollution and it's accumulating in the ecosystem causes serious risk to the environment and the living systems. Chromium, a common heavy metal contaminant, universally exists in soils, groundwater, and surface waters in trivalent and hexavalent forms with the widespread use in industrial processes, such as electroplating, metallurgy, leather tanning, and textile dyeing industries (Bhattacharya *et al.* 2014; Shen *et al.* 2010; Mu *et al.* 2015a; Zaleckas *et al.* 2013). Cr(III) is relatively harmless and immobile with a trace concentrations because it is needed for glucose metabolism in human nutrition as well as for plants and animals, whereas Cr(VI) is more toxic and moves through aquatic environments (Cao, Zhang 2006; Chen *et al.* 2015; Fang *et al.* 2011a). Cr(VI) with the property of being strong oxidizing agent, which can be absorbed to human body and result in inherited gene defects, cancer, and even death due to its detrimental characteristics such as carcinogenicity, mutagenicity, and teratogenicity (Shen

et al. 2010; Kim *et al.* 2015; Li *et al.* 2008). Thus, ever-increasing endeavors have been devoted to investigate the reduction of Cr(VI) to Cr(III) because it is a feasible method for removal of Cr(VI).

Engineered nanomaterials are newly developed for Cr(VI) removal, by which Cr(VI) was reduced, immobilized, and further removed by precipitation (Mu *et al.* 2015a, 2015b; Fang *et al.* 2011a). As a reductive material, nanoscale zero-valent iron (NZVI) has been used increasingly for removing a wide variety of pollutants including Cr(VI) over the last decade (Xu, Wang 2011; Kim *et al.* 2008; Ling *et al.* 2015). Due to its excellent physical and chemical properties (including large specific surface area, high reactivity, and low-cost), NZVI was chosen to be remediation agent for treatment of Cr(VI) wastewater. The NZVI particles reduce toxic heavy metals through oxidation of the Fe⁰ core and subsequent allocation of electrons to the pollutant at a relatively fast reaction rate because of its larger specific surface area and higher surface reactivity (Wang *et al.* 2008; Shu *et al.* 2007, 2010; Shih *et al.* 2011; Qiu *et al.* 2013). Although NZVI

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is very effective for environmental remediation, the agglomeration and instability of NZVI in the preparation and application process might diminish its reactivity. To obtain more physical stable NZVI particles, surfactants, starch, chitosan, carboxymethyl cellulose, resin, activated carbon, and microfiltration films have been studied as dispersant or support for preparing NZVI particles in aqueous media (Horzum *et al.* 2013; Lin *et al.* 2009; Lv *et al.* 2012; Meng *et al.* 2011). In addition, accompanying the increasing application of NZVI particles, more and more nanoparticles have been released into the aqueous environment and brought potential harmful impact on indigenous organisms, thus a new problem emerged, that of the nanotoxicity. However, the common dispersant did not play the role of preventing the release of nanoparticles into the environment. To overcome the aforementioned problems, the preparation method of NZVI-PVDF hybrid films with cation-exchange function was provided in this study for reductive transformation of Cr(VI).

As an alternative, NZVI particles supported on a special hybrid film may offer a successful resolution to this problem, because this material will (1) reserve NZVI particles in the film to avoid the risk for ecosystem, (2) be an ideal reaction media for controlling agglomerated and monodisperse nanoparticles, and (3) reduce material waste with its own performance of reusability (Wang *et al.* 2008; Yang *et al.* 2014). Polyvinylidene fluoride (PVDF) microfiltration films has been intensively studied for its applications to water and wastewater treatment in recent years (Byun *et al.* 2013; Li *et al.* 2010, 2013; Oh *et al.* 2009; Dong *et al.* 2013) for their open structure, 100–500 nm pore size, mechanical strength, and chemical stability, while showing no adsorption of metal ions (Xia *et al.* 2012; Fang *et al.* 2015). Researchers managed to immobilize nano particles in ion exchange (chelating) modified film to capture metal cation (Wang *et al.* 2008). Consequently, the secondary pollution can be avoided due to the ability of chelating to recapture the metal ions released after reaction, and the reuse of film is possible. Therefore, it is necessary to further investigate the activity of various types of NZVI-PVDF composite film for removal of different pollutants.

We aim to design an effective method for preparation and immobilization of NZVI at low-cost, with easy operation and environmental-friendliness. In this regard, poly acrylic acid (PAA) coating layer on the laboratory-synthesized support PVDF film was obtained by in situ polymerization of acrylic acid, contains carboxylic acid groups that can bind cations via ion exchange, chelation and static binding. After being functionalized by PAA, a nanoscale reactor was installed and NZVI particles were immobilized inside it. The objectives of current study are: (1) to fabricate PAA/PVDF-NZVI (PPN) hybrids for investigation of their reactivity toward heavy metals by

using Cr(VI) as a model; (2) to evaluate their efficiency for Cr(VI) removal under different Cr(VI) concentrations, pH values, and solution temperatures; (3) to calculate the activation energies of pristine NZVI and PPN hybrids to further study the reduction of Cr(VI); (4) to provide an innovatively revised kinetic and the possible transformation pathway of Cr(VI) by PPN hybrids. Considering these objectives, synthetic procedures, characterization, and discussion on the possible mechanism for the reduction of Cr(VI) by PPN will be presented.

1. Materials and methods

1.1. Materials

PVDF (FR 904, MW: 600,000) was supplied by Shanghai 3F New Materials Co. Ltd. China. Acrylic acid (AA, >99.5%) was obtained from Tianjin Yongda Stainless Steel Co., Ltd. Ethylene glycol (EG, >99%), ferrous sulfate heptahydrate and potassium borohydride were supplied by Chengdu KeLong Chemical Co., Ltd. Polyvinylpyrrolidone (PVP), dimethylacetamide (DMAc), ammonium persulfate (APS) and a mixture of ultrapure (UP) water (resistivity >18.25 M Ω cm) and ethanol were used as the non-solvents in the polymer precipitation. All chemicals in this study were obtained from Sinopharm Chemical Reagent Co., Ltd (China). All chemicals were used as received without further purification unless otherwise mentioned.

1.2. Preparation of PVDF microporous film

The phase-inversion method was used to prepare PVDF support film. PVDF (10%, wt.%) was dissolved into DMAc solvent at 298 K. Subsequently, PVP used in pore-forming were simultaneously introduced into the solvent, followed by vigorous magnetic stirring for at least 12 h for complete admixture. The casting polymer solution was deposited undisturbed for 24 h to take air bubbles away. To prepare a uniform liquid film, an appropriate amount of the casting polymer solution was uniformly dispersed on a glass plate at room temperature and 60% humidity. After exposed to air for 50 s, it was immediately immersed into the coagulation bath containing 20% aqueous ethanol. The porous PVDF film was formed by the diffusion of DMAc from the solvent phase (the polymer solution) to the non-solvent phase (the coagulation bath). The quadrate modified PVDF film (50×50×0.4 mm) was washed with distilled water and conserved in distilled water until it was functionalized with PAA.

1.3. Preparation of PAA/PVDF film (PP)

The prepared PVDF films were directly functionalized by in situ polymerization of AA on their surface as follows: (1) the PVDF films were pretreated by soaking in ethanol and UP water for 60 min and 24 h, respectively; (2) drying the PVDF films at 318 K for 90 min and cooling them to

room temperature (298 K); (3) a piece of treated film was immersed in AA polymerization solution for 10 min, then quickly sandwiched by two teflon plates and followed by placing them in a vacuum drying oven at 383 K for 14 h. The AA polymerization solution for modifying PVDF films was composed of AA (~49.1 wt%, monomer), EG (~2.5 wt%, cross-linking reagent), APS (~1 wt%, initiator) and UP water. The APS was first dissolved in UP water, then adding AA and EG into the resultant solution in order; (4) after the reaction, the teflon plates were taken out of the vacuum and released, next the PAA functionalized PVDF film was dipped in UP water for 2 days to remove surplus monomers and non-anchored polymers at room temperature, while the UP water was refreshed frequently; (5) the functionalized PVDF film by PAA was dried at 318 K for 90 min, after which cooled to room temperature for subsequent characterization and NZVI synthesis.

1.4. Synthesis of PPN hybrid

In details, the synthesized PAA/PVDF films were firstly immersed into 25 mL of NaCl (2 M) in a mixture of ethanol-water (V:V = 1:10) in a pH 11 and shaken back and forth at 30 rpm for 12 h under ambient temperature. After rinsing with UP water to remove the excess NaCl, the film containing $-\text{COONa}$ was then introduced into glass vials containing 50 mL of $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ (30, 60, or 120 mM) in ethanol-water (V:V = 2:5) solutions in a pH 4 with shaking at 30 rpm for 14 h at room temperature, where Na^+ was exchanged for Fe^{2+} . Next, the yellowed films were rinsed with UP water again and finally immersed into 40 mL of NaBH_4 (0.8 M) in the mixture of ethanol-water (V:V = 1:10) for 40 min to yield NZVI particles supported on the PAA/PVDF film. The process of PVDF film preparation, PPN hybrids synthesis and PPN hybrids regeneration was shown in Figure 1.

1.5. Batch experiments

Cr(VI) removal was conducted in 60 mL glass vials and each of which contained 50 mL of Cr(VI) solution. All experiments were conducted in triplicated under aerobic conditions by shaking back and forth at 150 rpm with a rotary shaker. One piece of PPN hybrid film was loaded into each reaction vial. At regular time intervals (up to 120 min), 5 mL of reaction samples were withdrawn for Cr(VI) residue analysis with atomic absorption spectrophotometer. An identical procedure was used to remove Cr(VI) with freshly prepared bare NZVI (namely BN) only for comparison. In addition, parallel blank experiments were also conducted under the same conditions, with one piece of PP film only, to examine whether the adsorption of PP hybrid films would affect the removal of Cr(VI) or not. Subsequently, a series of degradation experiments were also carried out under different initial concentrations of Cr(VI) solution and pH values to optimize the reaction conditions of Cr(VI) removal by PPN. The removal experiments under different reaction temperatures were used to calculate the activation energies.

1.6. Characterization

The surface morphologies of freshly prepared PVDF and modified PVDF films with nanoscale Fe^0 particles were scanned by a QANT200F SEM system (FEI Co., USA). The film samples were coated with a thin layer of gold to improve their electrical conductivity prior to being scanned. The Fourier Transform Infrared spectra of the bare PVDF and PAA-functionalized PVDF films were recorded on a Varian 7000 e FTIR with attenuated total reflectance (ATR). Films were dried at 363 K for 4 h before testing. All FTIR data of PVDF films were collected using 128 scans at a resolution of 4 cm^{-1} .

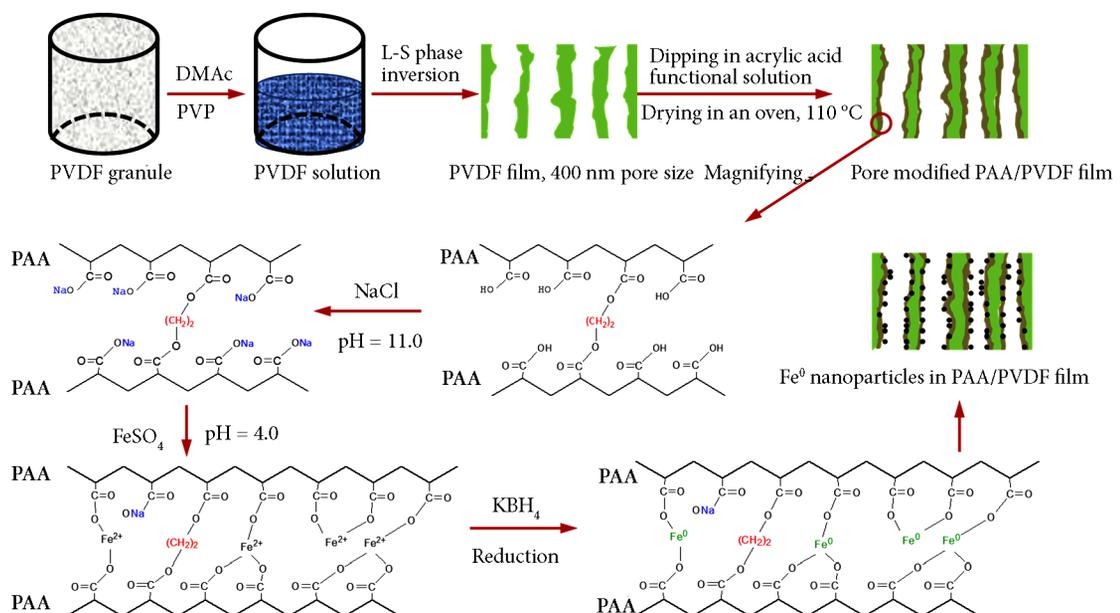


Figure 1. The process of PVDF film preparation and PPN hybrids synthesis

2. Results and discussion

2.1. Surface functionality of PPN using FTIR spectra

FTIR-ATR spectroscopy was used to distinguish different organic groups on the PVDF films with PAA and bare PVDF (Figure 2). Absorption peaks at 2800–3100 cm^{-1} assigned to the hydroxyl group stretching and vibration modes of $-\text{COOH}$ appeared in the spectra of the PAA

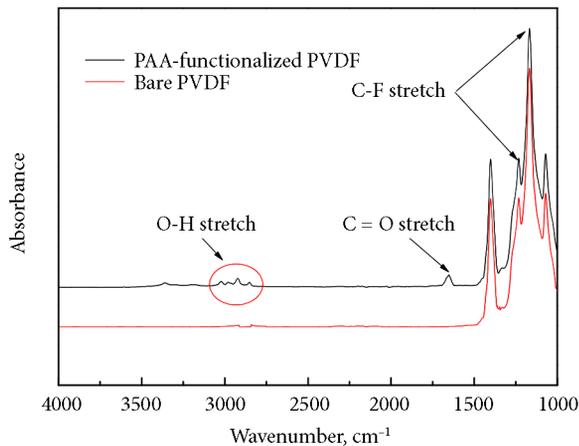


Figure 2. FTIR spectrum for bare and PAA-functionalized PVDF films

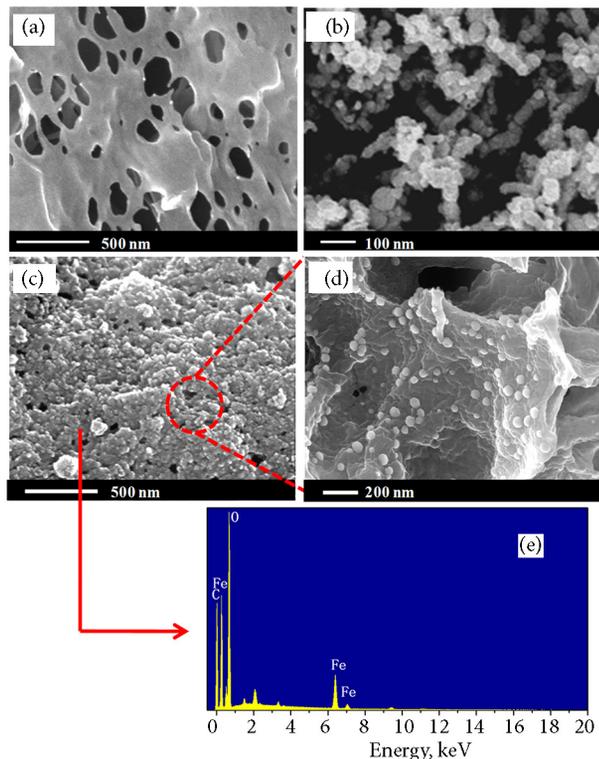


Figure 3. SEM images of PAA/PVDF film surface (a), NZVI particles before immobilization on the film surface (b), NZVI particles supported on PAA/PVDF films (c); high-magnification of modified PVDF film containing nanoscale Fe^0 particles (d), and electron diffraction spectroscopy elemental analysis (e)

modified PVDF films. The FT-IR spectra also showed that the 1680 cm^{-1} absorption peak of the film after PAA functionalized was appeared obviously, which is not present in the spectrum for the bare PVDF film. This peak is attributed to the presence of C–O bond stretching in carboxylic acid groups. The existence of the above two kinds of peaks on the PAA modified PVDF films indicating successful PAA immobilization within the functionalized film. Hence, the film hydrophilicity was controlled better because that AA reacted with the hydroxyl groups on the modified film. The absorption peaks at 1140–1280 cm^{-1} were found to be intense both in the bare PVDF film and modified PVDF (Dai *et al.* 2014), which were assigned to C–F bond stretching vibrations in PVDF.

2.2. PVDF Surface coverage of NZVI particles in SEM images

The surface morphologies of freshly prepared PAA/PVDF film, nanoscale Fe^0 particles before immobilization on the film surface, nanoscale Fe^0 particles supported on PAA/PVDF film, and high-magnification of modified PVDF film containing NZVI particles are shown in Figure 3. The PAA/PVDF film (Figure 3a) showed great porosity with a highly nonuniform porous microstructure (100–400 nm) by the phase inversion process and grooves are obtained. As observed in SEM image of the porous film surface, after being modified by PAA, the PAA layer did not diminish the surface pore size anymore comparing with PVDF film. The SEM image of nanoscale Fe^0 particles before immobilization on the film surface is shown in Figure 3b. Compared with immobilized NZVI, severe aggregation of unimmobilized NZVI could be found. Nanoscale Fe^0 particles were immobilized on the surface (Figure 3c) of PAA/PVDF film, indicating that PAA was able to transport the NZVI into the pores of the PVDF film and increase the Fe^0 loading. An inspection of the particle size by SEM at a higher magnification showed that the NZVI were well immobilized on the surface of the support even in the porous. Therefore, the PAA/PVDF film fresh prepared in this study is considered to be a good matrix for immobilizing nanoscale Fe^0 particles. Simultaneously, electron diffraction spectroscopy (EDS) was employed to analyze the surface element composition of the PPN. As shown in Figure 3e, NZVI were found to be successfully immobilized on the PAA/PVDF film.

2.3. Removal of Cr(VI) by various materials

The typical removal profiles of Cr(VI) against time on PP, BN and PPN materials are depicted in Figure 4. In the absence of any materials, no measurable Cr(VI) loss was observed. However, the residual concentration of Cr(VI) steadily decreased when PPN hybrid were introduced into the solutions, indicating that nanoscale Fe^0 particles were responsible for all the losses of Cr(VI). For example, more than 96% of Cr(VI) was removed by PPN3 within 120 min in a solution of pH 3.88. This was the maximum

removal of Cr(VI) that could be obtained for PPN hybrid under the conditions. Comparatively, only 44% of Cr(VI) was reduced using 7 mg of BN under the similar conditions, which was lower than that by PPN1 only containing 3.22 mg of NZVI. This implies that in comparison to BN, a smaller amount of NZVI immobilized on PP could perform the same removal efficacy in a shorter period of time, thus saving time as well as materials. The superior removal characteristics of PPN over BN may be ascribed to the fact that, the PP hybrid films with tiny nano-reactors as support materials, i.e., the charged $-\text{COO}-$ groups of PAA gels inside PVDF films, did control NZVI agglomeration, thus enhancing the reactivity of PPN hybrid toward Cr(VI). The change in Cr(VI) reduction with varying Fe loadings indicated that there was an increase in the removal with an increase in the loading of NZVI embedded in PPN. In the case of PPN hybrids, the Cr(VI) removal percentage increased sharply from 0 min to 20 min, while

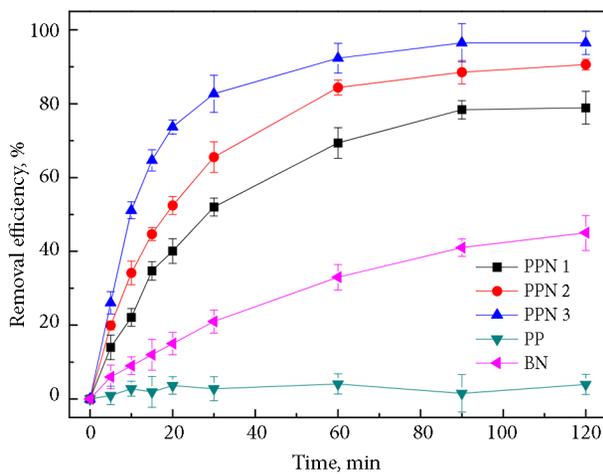


Figure 4. Removal of Cr(VI) by PP, PPN, and BN. The Fe^0 loadings of PPN1, PPN2, and PPN3 are 3.22, 4.85 and 6.36 mg, respectively, and the dosage of BN is 7 mg ($\text{pH} = 3.88$, $C_{\text{Cr(VI)}} = 20 \text{ mg L}^{-1}$)

increased at a slow pace beyond 20 min. This is because within a reaction time of 20 min, PPN could supply abundant reactive sites for Cr(VI) reduction. However, beyond 20 min, such reactive sites would be covered by the iron hydroxides or oxides formed on the surface of PPN during the reaction, thus resulting in declined efficacy of Cr(VI) reduction by PPN. Additionally, it was also found that the PP hybrids showed little adsorption of Cr(VI) at less than 4% after 120 min, which indicating the sorption of PP hybrid films did not contribute to the removal of Cr(VI).

2.4. Influencing factors

For further investigation of the effects on the removal efficiency of Cr(VI) by PPN hybrids, initial concentration of Cr(VI) and solution pH were also examined (Figure 5). Figure 5a depicts the effect of initial Cr(VI) concentration on the removal of Cr(VI) in a range of 10–50 mg L^{-1} . Generally, the removal efficiency of Cr(VI) increases with the decrease of the initial Cr(VI) concentration C_0 , which is mainly responsible for the increase of total available active sites for Cr(VI) removal with the decreasing concentration of Cr(VI), thereby leading to higher reaction efficiency. For example, the removal efficiency of Cr(VI) by PPN2 increased from 59.26% to 96.32% within 120 min in a pH 3.88 reaction solution when the C_0 of Cr(VI) decreased from 50 mg L^{-1} to 10 mg L^{-1} . The effect of solution pH on the reaction is shown in Figure 5b. Obviously, the removal efficiency of Cr(VI) by PPN increased with the decreased initial pH. For instance, the removal of Cr(VI) increased when solution pH decreased from 9.21 to 3.88. This is due to that the active species like H^* will be consumed when Cr(VI) was reduced by PPN. Decreasing initial solution pH is beneficial to the corrosion reaction of Fe^0 with water (i.e., the formation of H^* species) and making against the formation of passive ferrous oxide/hydroxide, thus both the needed reactant (i.e., active hydrogen) and reactive sites for Cr(VI) removal were supplied, therefore improving the removal efficiency of Cr(VI).

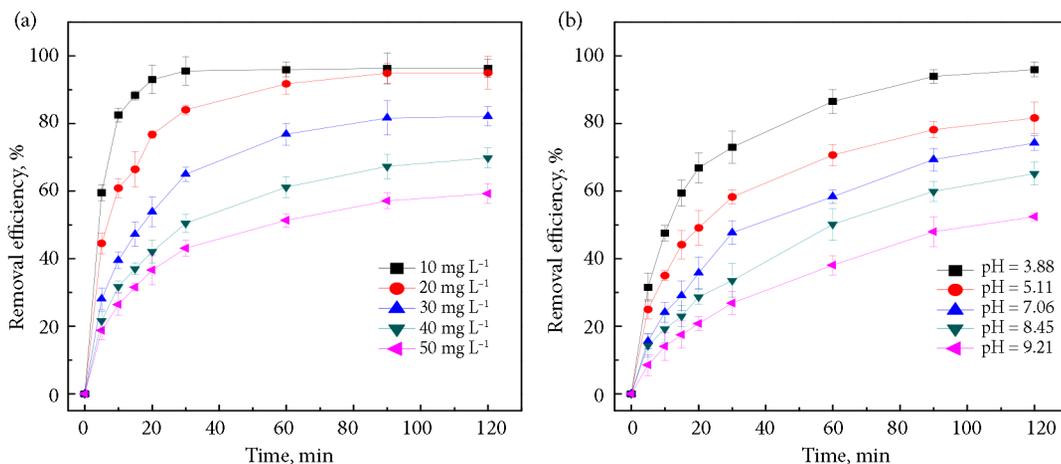


Figure 5. Removal of (a) various initial concentrations of Cr(VI) by PPN2 ($\text{pH} = 3.88$, temperature 298 K) and (b) 20 mg L^{-1} of Cr(VI) by PPN2 under various pH values (temperature 298 K). Other reaction conditions: volume 50 mL and reaction time 120 min.

2.5. Stability and reusability of PPN

There is another important concern for NZVI-centered remediation except how to inhibit its aggregation and improve its mobility during synthesis, which is how to avoid its potential release into ecosystem and recover it using simple regeneration procedure over the whole course of its application. It's necessary and practical to recycle and regenerate the PPN hybrid for evaluating the long-term performance of PPN hybrid for environmental remediation and reducing the cost of PVDF film. Briefly, the aged PPN was first immersed in UP water for 12 h, while the UP water was refreshed frequently. Then the PPN hybrid was dried at 313 K for 60 min. Subsequently, the cooled PPN was dipped into 40 mL of KBH_4 (0.8 M, the mixture of ethanol-water (1:10, v/v)) prepared for 40 min, followed by washing it with UP water for 3 times. After that, the regenerated PPN hybrids were used to remove Cr(VI) from water. The removal efficiency of Cr(VI) by

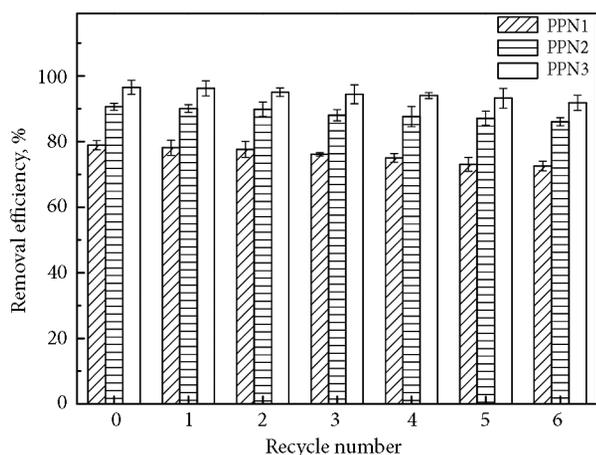


Figure 6. Cr(VI) removal with recycle numbers for the regenerated PPN. Reaction conditions: 50 mL of 20 mg L⁻¹ Cr(VI) solution, pH = 3.88, reaction time 120 min, and solution temperature 298 K

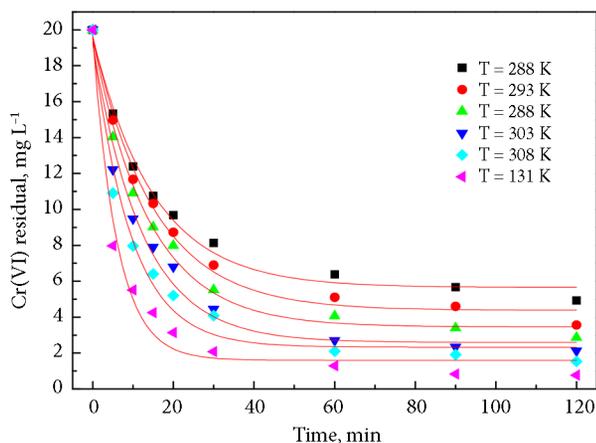


Figure 7. Removal of Cr(VI) by PPN2 at different temperatures. Reaction conditions: 50 mL of 20 mg L⁻¹ Cr(VI) solution, pH = 3.88, and reaction time 120 min. Lines represent the two-parameter pseudo-first-order decay model

regenerated PPN hybrids in each cycle is shown in Figure 6. Obviously, the reactivity of the regenerated PPN hybrids toward Cr(VI) was not appreciably deteriorated after 6-cycle use compared with that of freshly prepared ones, suggesting that the hybrid PPN with insignificant loss of reactivity retained most of the capacity for supporting nanoscale iron particles after being renewed. May be it's potentially employed to remove Cr(VI) from aqueous environment during its long-term application.

2.6. Reaction kinetics and pathways

Evaluating reaction kinetics of NZVI-contaminate system is a considerable much aspect to well understand the application of NZVI in environment. So variation of experimental factors of reaction temperature indicated that Cr(VI) removal by NZVI could be optimized for effective transformation of Cr(VI) in aqueous solution. Some references reported that the reaction of pollutants with NZVI could be described by a first-order or pseudo-first-order kinetics (Jiang *et al.* 2012; Fang *et al.* 2011b, 2011c). However, some other studies indicated that a two/three-parameter pseudo-first-order decay model could well describe the above reaction process, because it took the loss of available reactive sites and presence of nonreactive pollutants into account (Shu *et al.* 2007, 2010). In order to have in-depth understanding of the reactive process and kinetics, batch experiments of Cr(VI) removal by PPN2 was carried out under different temperatures (Figure 7). On the basis of the removal profiles of Cr(VI) in current study, the first-order or pseudo-first-order kinetics model was found doesn't provide the best fit with the experimental data the removal of Cr(VI) over PPN as we see that the Cr(VI) in solution generally experienced a fast decline within the first 20 min and then gradually level off at a relatively constant concentration, indicating the presence of nonreactive Cr(VI) in the reaction solution. Considering the residual nonreactive Cr(VI), a two-parameter pseudo-first-order decay model was used to describe the reaction kinetics in this study:

$$C_t = C_{ultimate} + (C_0 - C_{ultimate}) \times \exp(-kt), \quad (1)$$

where C_t stands for the Cr(VI) concentration (mg L⁻¹) in solution at reaction time t ; $C_{ultimate}$ represents the concentration of nonreactive Cr(VI) (mg L⁻¹) in solution at infinite time in this study; C_0 is the initial concentration of Cr(VI) (mg L⁻¹); and k represents the reaction rate constant. The values of $C_{ultimate}$, k calculated, and other conditions are given in Table 1. Obviously, the two-parameter pseudo-first-order kinetics model provides the best fit with the experimental data, and the R^2 are ranged from 0.9265 to 0.9868. A high k with decrease of $C_{ultimate}$ indicates that the Cr(VI) can be effectively removed by PPN. Such a kinetics model for the reaction is reasonable, which might be attributed mainly to the reactive sites provided by PPN were not necessarily excessive and suffered a corresponding loss over the removal process of Cr(VI).

To reveal the control step of the whole reaction, activation energy of a certain chemical reaction was investigated. It has been shown that diffusion controlled reaction usually has relatively low activation energy (8–21 kJ mol⁻¹), while the surface-control reactions have relatively higher activation energy (>29 kJ mol⁻¹) in previous study. Here a manipulated Arrhenius equation was introduced to describe the relationship between the k and temperature according to the k data obtained from the slope of the fitting line under different temperatures.

$$\ln k = -\frac{E_a}{RT} + \ln A, \quad (2)$$

where E_a represents the activation energy (kJ mol⁻¹), A represents a frequency factor, R represents the ideal gas constant (kJ/mol K), and T represents the reaction temperature (K). Thus, a linear correlation will be resulted from a plot of $\ln k$ versus $1/T$ according to Eq. (2). Figure 8 shows the plot of $\ln k$ versus $1/T$ for Cr(VI) removal by PPN2. The activation energies (gained from the slopes (E_a/R)) of Cr(VI) by PPN2 was 35.17 kJ mol⁻¹, suggesting that the Cr(VI) removal by PPN2 can be considered as a surface controlled chemical reaction. Conversely, the activation energy of Cr(VI) reduction with pristine NZVI was 46.31 kJ mol⁻¹, indicating that the NZVI supported by PAA/PVDF films result in a lower activation energy, and that a faster chemical process during the Cr(VI) reduction by pristine NZVI can be anticipated through the approach of Cr(VI) immobilization with PAA/PVDF films.

It's well known that the removal of heavy metals by NZVI is a surface-mediated process. Such surface-mediate process as PPN-Cr(VI) reaction also involves several steps as follows (Figure 9): (1) diffusion of Cr(VI) molecules into PPN surface, (2) adsorption onto reactive sites provided by PPN, (3) electrons directly or H^{*} species indirectly via the oxidation of NZVI with H₂O inducing the chemical reaction, and (4) diffusion of products from reactive PPN.

Conclusions

Nanoscale zero-valent iron particles (NZVI) were successfully immobilized in the PAA/PVDF film (PPN) for removal of Cr(VI). SEM characterization of PPN indicates that the synthesized nanoscale zero-valent iron particles were homogeneously dispersed in the film. The PPN

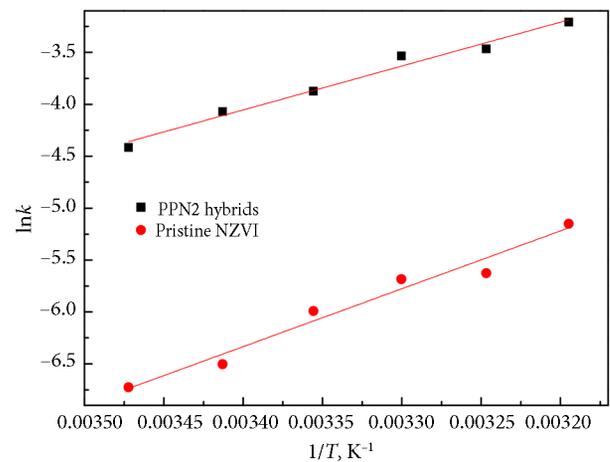


Figure 8. Arrhenius plot for the estimation of activation energy: Cr(VI) removal by PPN2 hybrids and pristine NZVI

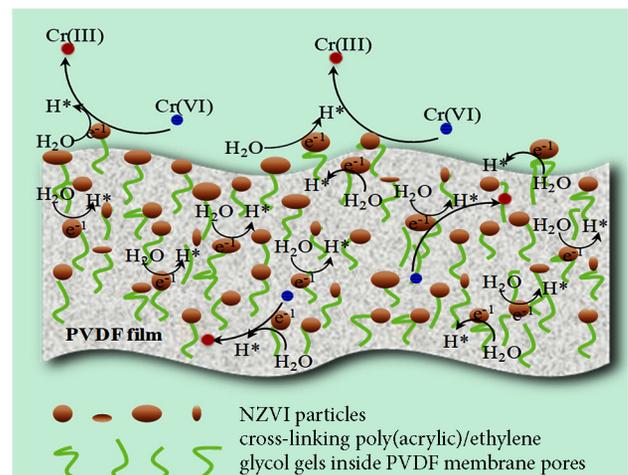


Figure 9. Conceptual model for possible removal pathways of Cr(VI) by PPN

hybrids demonstrated the highest removal efficiency of Cr(VI) removal with different materials (PP, PPN and BN). The experimental results show that only 44% of Cr(VI) was removed by using 7 mg of unimmobilized NZVI under the same reaction conditions, which was lower than that by PPN1 only containing 3.22 mg of NZVI. Comparing with the pristine NZVI, activation energies of PPN

Table 1. Fitted data for the removal of Cr(VI) by PPN using a two-parameter pseudo-first-order decay kinetics model

C_0 (mg L ⁻¹)	Initial pH	Temp. (K)	Removal (%)	$C_{ultimate}$ (mg L ⁻¹)	k (min ⁻¹)	R^2
20	3.88	288	75.33	4.934	0.0121	0.9868
20	3.88	293	82.21	3.558	0.0171	0.9716
20	3.88	298	85.69	2.862	0.0208	0.9731
20	3.88	303	89.36	2.128	0.0292	0.9591
20	3.88	308	92.30	1.540	0.0313	0.9265
20	3.88	313	96.15	0.770	0.0405	0.9805

are calculated to be $35.17 \text{ kJ mol}^{-1}$, indicating that Cr(VI) reduction process with PPN is a surface-controlled chemical reaction, and the NZVI supported by PAA/PVDF films result in a lower activation energy. Over all, the PPN hybrids exhibited high reactivity, excellent stability and reusability for Cr(VI) removal. Further studies revealed that decreasing initial concentration of Cr(VI), increasing reaction temperature and decreasing pH value accelerated the removal of Cr(VI) from aqueous solution. A two-parameter pseudo-first-order model was provided to analyze the reaction kinetics of Cr(VI) removal over PPN under various conditions. This study suggests that NZVI-PVDF hybrid possessing excellent performance may be a promising functional material for treatment of Cr(VI) contaminated wastewater.

Acknowledgements

This research is supported by the National Nature Science Foundation of China (NSFC, No.51368025, and No. 51068011).

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